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Techno-economics of the synthesis route from CO₂ and clean H₂ to polycarbonate polyols

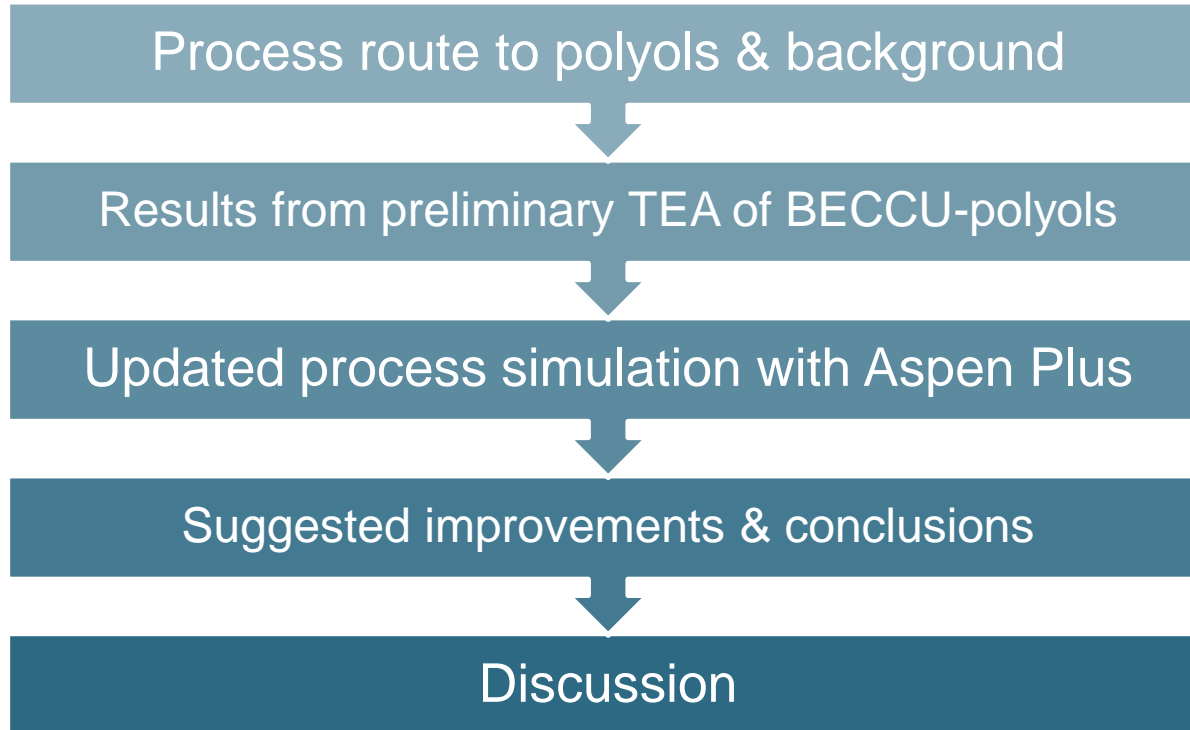
Miia Nevander
KEROGREEN Winter School
10.2.2022



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Agenda





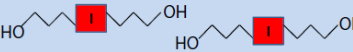
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Process route to polyols & background

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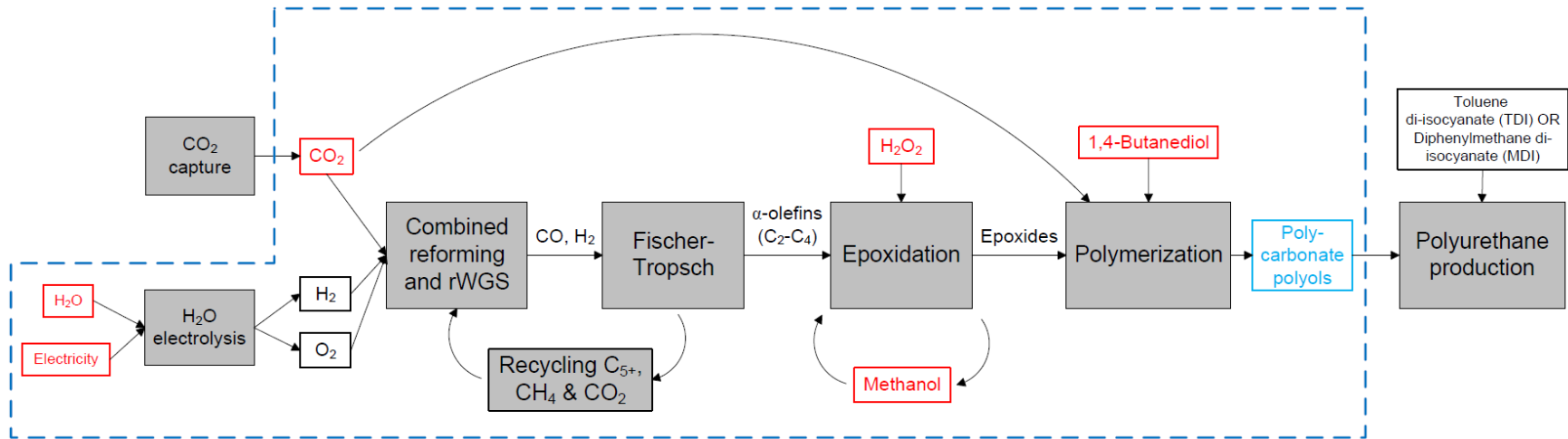
Polycarbonate polyols – high value chemicals and plastics

Term	Definition	Structural formula
Polycarbonate polyol	Low molecular weight polymer, linear aliphatic polycarbonate, derived from the copolymerization of carbon dioxide and an epoxide, containing two or more terminal hydroxyl groups (Qin & Wang, 2019)	<p data-bbox="1348 390 1702 416">Low Mw polyols (thermosets)</p> <p data-bbox="1348 437 1702 463">PO + CO₂ + Catalyst + Initiator</p>  <ul data-bbox="1348 550 1702 601" style="list-style-type: none"> • Initiator spurs polymerizations • Creates more, shorter PPC chains <p data-bbox="1348 626 1599 651">(Raschka et al., 2018)</p>

- High value product, selling price can be even 6 000 €/tonne
- Applications: polyurethanes, coatings, adhesives, ...

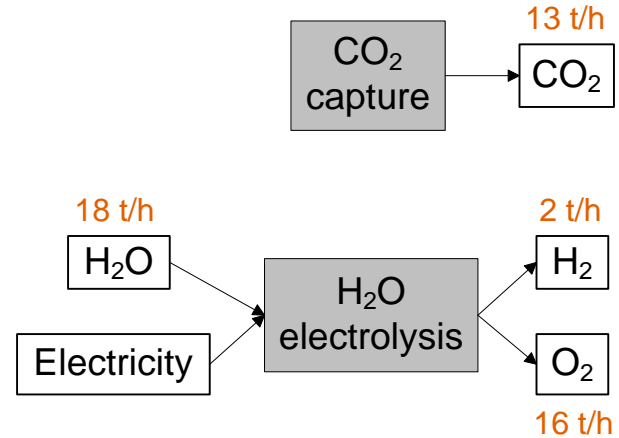
BECCU-polyols from biogenic CO₂ & green H₂

- The process is based on the **production of olefins** through reverse water-gas shift (rWGS) and Fischer-Tropsch (FT) reaction steps
- The olefins are further converted to epoxides through oxidation reactions by peroxides and epoxides are polymerized together with CO₂ to obtain polyols
- The yield of C₂-C₄ olefins is maximized to be used in polyol production



Carbon dioxide & hydrogen as starting materials

- CO₂ from biogenic sources with MEA
 - 50 €/tonne capture & processing cost assumed
- H₂ from alkaline electrolysis (AEC)
 - 100 MW electrolyser ($\eta=67\%$)
 - 60 M€ electrolyser & costs of water and electricity





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Results from preliminary TEA of BECCU-polyols

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Assumptions & results

Inputs	Price	Outputs	Price
Electricity (total)	45 €/MWh	Cyclic carbonates	900 €/t
Hydrogen peroxide	550 €/t	By-product heat	20 €/MWh
CO ₂ supply	50 €/t	By-product oxygen	40 €/t

Other parameters	
Electrolyser electricity input	100 MW _e
Annual plant operation time	8 000 h
Total investment cost estimate (20 years and 8% WACC for annuity)	124 M€

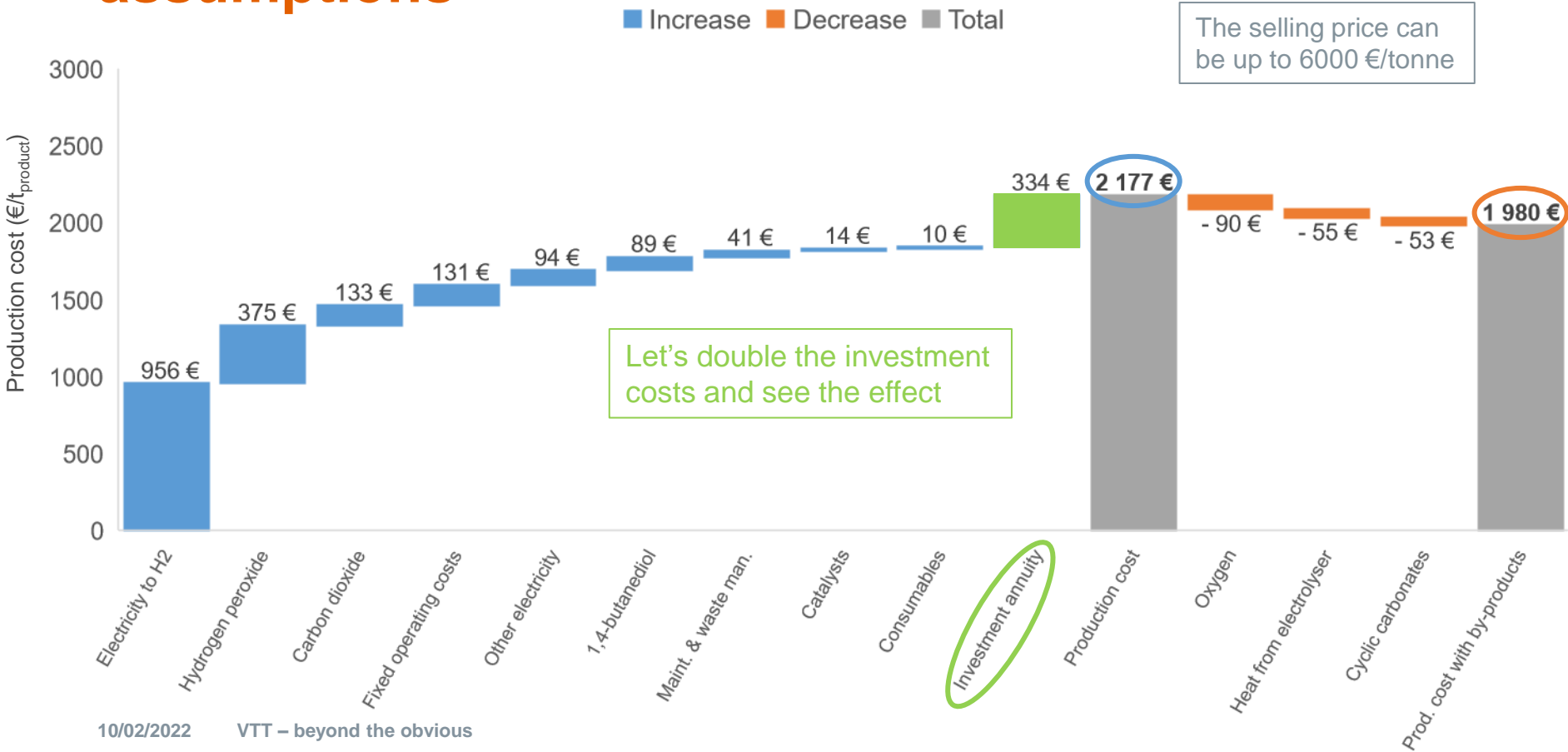
IN	
CO ₂ need	100 kt/a
H ₂ need	16 kt/a



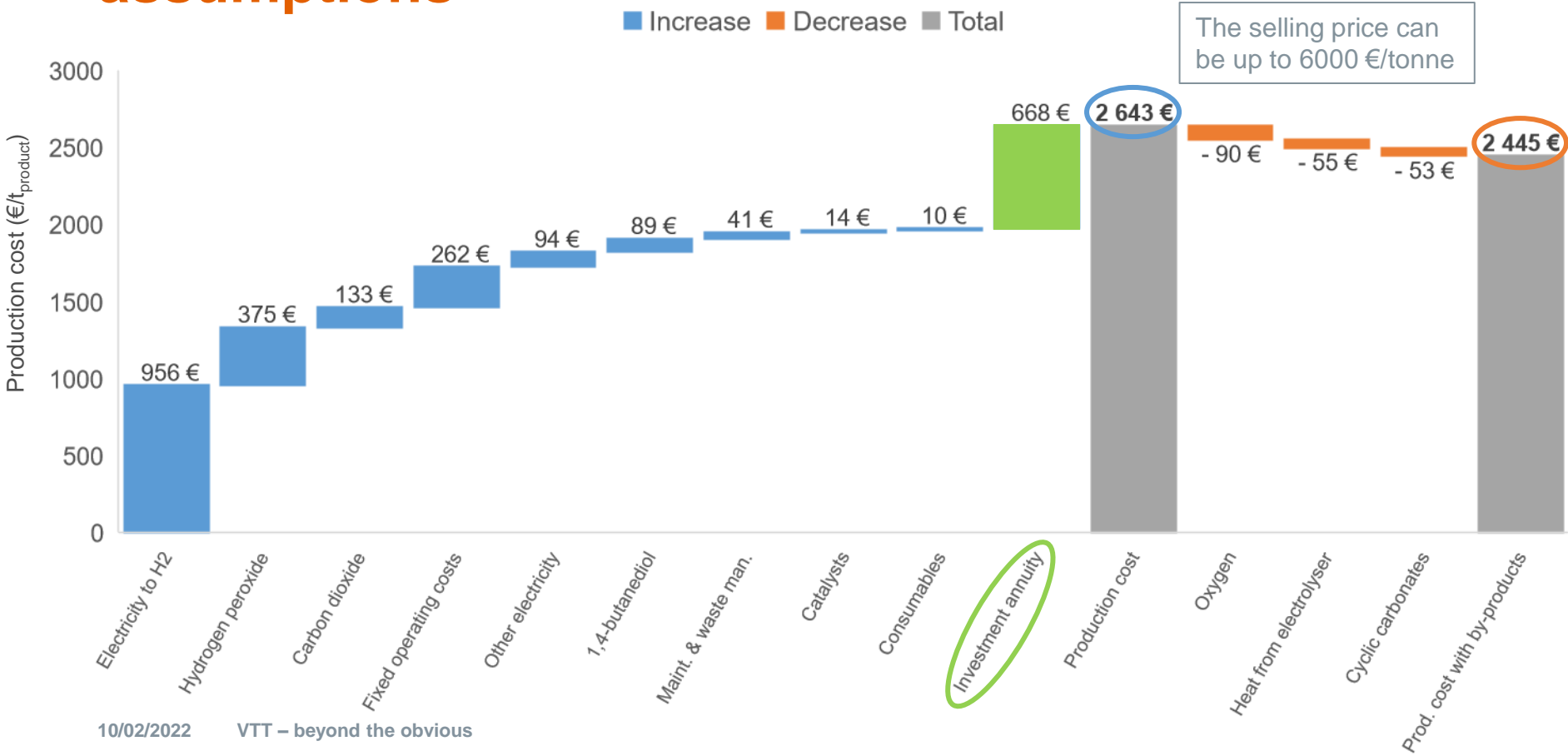
OUT	
Polycarbonate polyols	38 kt/a
Cyclic carbonates	2 kt/a
Excess oxygen	84 kt/a

Production cost estimation with preliminary assumptions

The selling price can be up to 6000 €/tonne



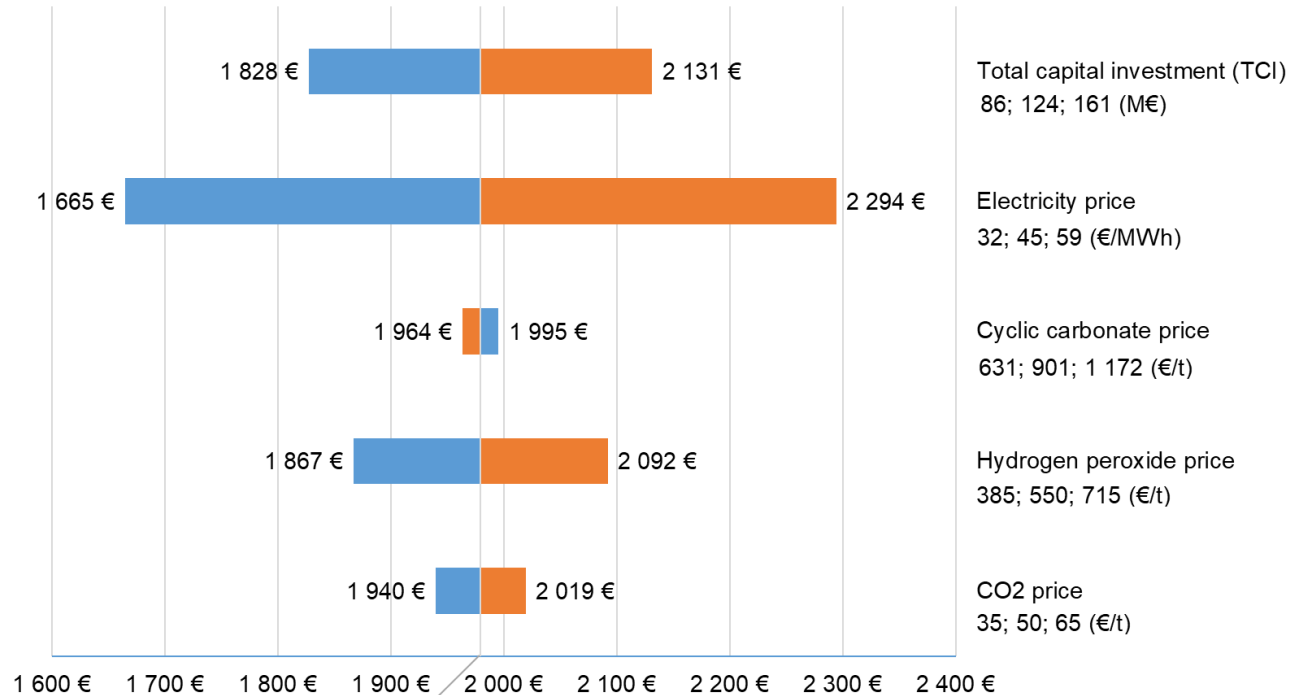
Production cost estimation with preliminary assumptions



The production costs are heavily dependent on the price of electricity

Effect of $\pm 30\%$ change in each variable to production cost

■ 30 % ■ -30 %





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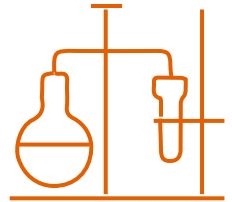
Updated process simulation with Aspen Plus

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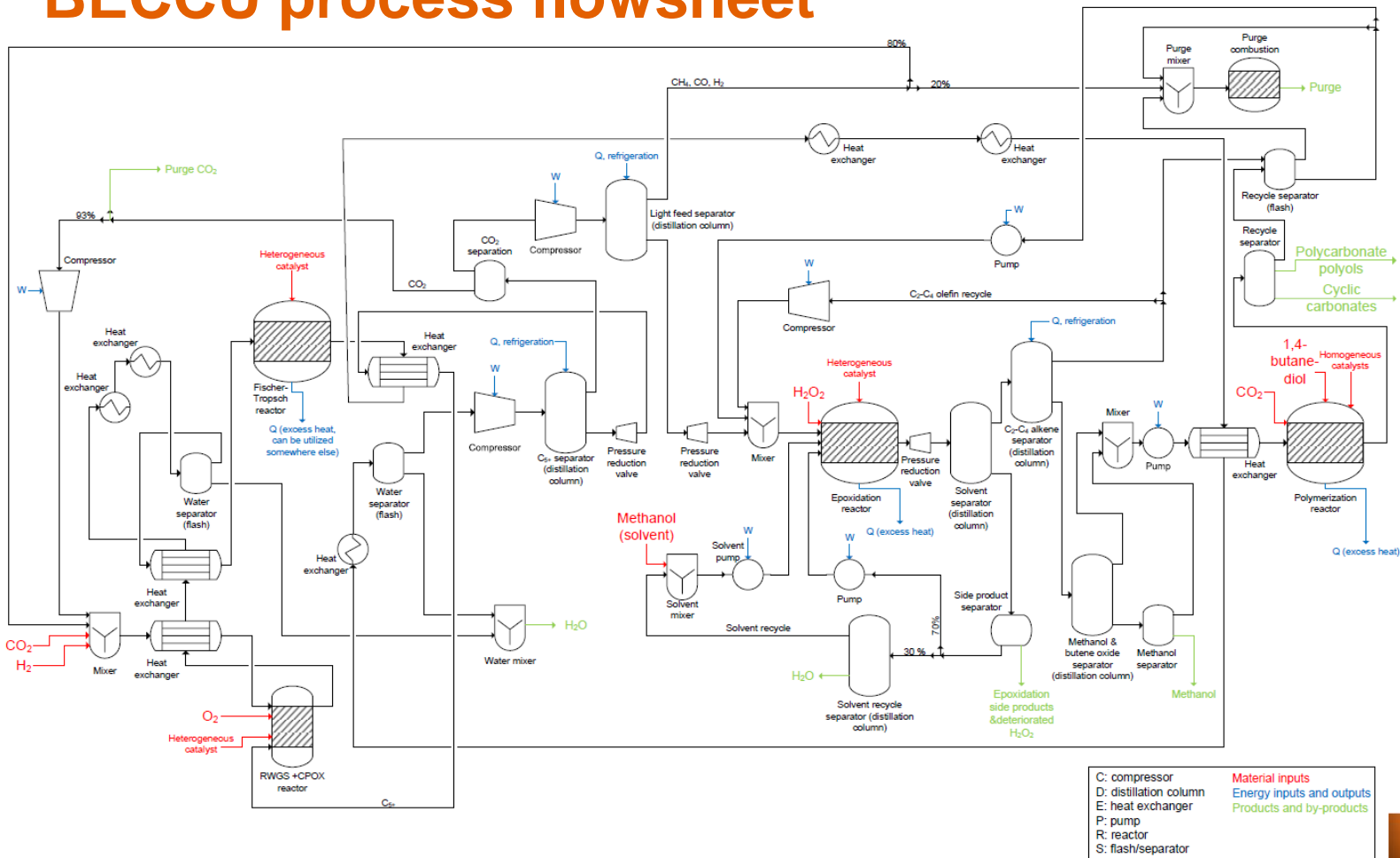


Simulation model improved since the preliminary TEA results

- Raw material in epoxidation, ethene, is difficult to separate from other light substances when there is CO₂ in the feed
 - CO₂ freezes in temperatures needed for cryogenic separation
 - We assume a separation method for CO₂ and are able to retrieve ethene to epoxidation
- Recycle loop added for epoxidation solvent (methanol)
 - Energy consumption of separations optimized
- Experimentally discovered side products have been added to the model
- Reactor performances have been revised and updated



BECCU process flowsheet





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Suggested improvements & conclusions

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Room for improvements after BECCU project

Separation of CO₂ after Fischer-Tropsch (FT)

- FT catalyst is both rWGS and WGS active, so there should be some CO₂ in the feed to FT
- Further investigation needed to find the most suitable separation method

Separation of side products of epoxidation

- Side products form azeotropes with methanol, water and other components, so the separation seems challenging

Epoxidation solvent (methanol) and product (1-butene oxide) have boiling points very close to each other, and they form azeotropes

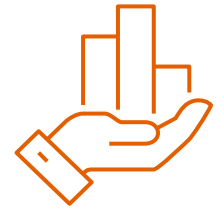
- Difficult to separate
- Liquid-liquid extraction process should be further investigated

The modelling of polycarbonate polyols

- Polymer modelling requires thermodynamic data
- The products are not added to Aspen model

Conclusions

- BECCU production route seems competitive & profitable
 - Production cost was found lower than the expected selling price
 - Sensitivity analysis showed that the process is most sensitive to changes in electricity price
 - TCI and H₂O₂ price have the second and third greatest effect
- An improved TEA is in the making, with the updated process model and experimental findings



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Questions & Discussion

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